


Research Article

Research on the development of Value-added Vinegar using Subcritical Treated Water

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Abstract

Sake lees and rice bran, which are residues from food processing, were liquefied by subcritical water treatment to effectively produce new vinegar. Our previous studies reported that high concentrations of amino acids can be recovered from sake lees treated with subcritical water at 120°C for 240 min [1,2]. In this study, the conditions for subcritical water treatment of rice bran were examined, and a liquefied product with a high liquefaction rate and high mineral content was obtained at 180°C for 30 min. Acetic acid fermentation was then conducted with a ratio of sake lees liquefied product to rice bran liquefied product of 1:1. The resulting vinegar had a high nutritional value similar to commercially available black vinegar.

Keywords: Biomass; Green chemistry; Subcritical water extraction; Vinegar

Introduction

Rice bran and sake lees, which are residues of the vinegar production process, contain large amounts of proteins and minerals. However, they are discarded in large quantities every year, thereby incurring significant costs. Against this background, previous studies have shown that these food production residues contain useful components [3-6]. Therefore, the authors focused on rice bran and sake lees, and the application of subcritical water treatment for their liquefaction to produce a product rich in amino acids and minerals, which can be used to produce new vinegar. The subcritical water used in this study refers to water in a liquid state at high temperature and high pressure, and it has the characteristics of being non-toxic, non-flammable, and non-explosive. In particular, the ionic product constant of subcritical water is high and acts like an acid or alkali catalyst, making it applicable to the hydrolysis of proteins in biomass, as reported in previous studies [7-9]. Sake lees, which is the raw material that is the focus of this study, is characterized by high protein and water contents, while rice bran is high in carbohydrates and minerals. In addition, previous studies have reported that high concentrations of amino acids can be recovered from sake lees by processing at relatively low temperatures of 120-140°C [1,2]. However, previous studies on subcritical water treatment of rice bran are limited; thus, this study focused on subcritical water treatment of rice bran. As a result, the authors conducted solid-liquid separation of the treated material after subcritical water treatment in the range of 120-160°C; however, successful separation was not achieved. It is possible that the polysaccharides were not hydrolyzed sufficiently and could not be separated by filtration. This indicates that rice bran may require treatment at a higher temperature because of its low water content and robust carbohydrate structure.

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Experimental

Materials and Standard reagents

Materials: Rice bran and sake lees provided by Maruboshi Vinegar Co. (Fukuoka, Japan) were used as raw materials, as shown in figure 1.

Standard reagents: Amino acid mixture standard solution (Type H). Calibration result is traceable to Primary Measurement Standards (National Standards) based on Measurement Law. Ammonium nitrogen standard solution (for water analysis). These were purchased from FUJIFILM Wako Pure Chemical Corporation (Osaka, Japan). Standard solutions for calcium, magnesium, potassium, and sodium were purchased from FUJIFILM Wako Pure Chemical Corporation. Calibration result is traceable to Primary Measurement Standards (National Standards) based on Measurement Law.

Experimental apparatus and procedure

The experimental equipment and methods are published in our previous paper [1,2]. An autoclave was to generate high temperature and high pressure (shown in figure 2). The reactor was constructed from SS 316 steel and has an internal volume of 500mL. The reactor was charged with 45 g of raw material and 300 mL of distilled water, mixed with a stirrer, and then sealed. Thereafter, the temperature was raised to a predetermined setpoint (180-220°C) by a band heater installed in the reactor. The heating time was 15 to 30 min. After reaching the predetermined temperature, the contents were reacted for 30-240 min while stirring at 300 rpm. The pressure in the reactor varied from 1.3 to 2.6 MPa depending on the vapor pressure of water and the product gas evolved during processing. After the subcritical water treatment, the band heater was removed from the reactor and a fan was used to quickly quench the reactor. After the reaction solution was sufficiently cooled (hereinafter this solution will be referred to as a sub-critical water treatment solution) was collected and separated into filtrate and water-insoluble components by suction filtration.



Figure 1: Raw materials used in this study

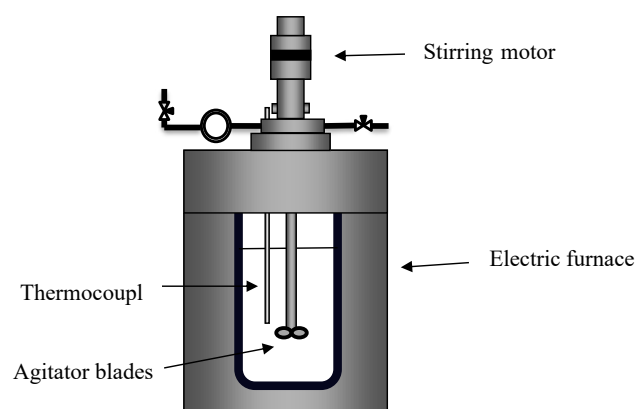


Figure 2: Diagram of the batch reactor used in subcritical treatment

Analysis

The following sections describe how each obtained filtration residue and aqueous solution was analyzed, and the methods used to quantitatively analyze the concentrations of amino acids, nitrogen, phosphorus, and minerals contained in the subcritical water treatment solution.

Amino acids: Amino acids were derivatized with 3-mercaptopropionic acid [MPA] and o-phthalaldehyde [OPA] and separated by a column [2.6 μ Kinetex EVO C18 100×3 mm; SHIMADZU GLC (Tokyo, Japan)] for ultra high-speed analysis, then analyzed by high performance liquid chromatography (HPLC) with a fluorescence detector (NEXERA X 2; SHIMADZU (Kyoto, Japan)). Eighteen amino acids were isolated, as shown in table 1.

Table 1: Amino acids quantitatively analyzed in this study.

1. Aspartic acid	2. Glutamic acid	3. Serine	4. Histidine
5. Glycine	6. Threonine	7. Arginine	8. Alanine
9. GABA	10. Tyrosine	11. Valine	12. Methionine
13. Cystine	14. Tryptophan	15. Phenylalanine	16. Isoleucine
17. Leucine	18. Lysine		

*GABA: 4-aminobutyric acid

Total amino acid content (mg/L) = Total of 18 amino acids (mg/L)

Total nitrogen concentration: Total nitrogen (mg/L) was analyzed using the Kjeldahl method [10].

Ammonia nitrogen concentration: Ammonia nitrogen (mg/L) was analyzed using the indophenol method [11].

Phosphorus concentration: Phosphorus (mg/L) was analyzed using the molybdenum-blue method [12].

Mineral concentration: Potassium, calcium, and magnesium (mg/L) were quantitatively determined by atomic absorption spectrometry (AA-7000; SHIMADZU).

Liquefaction rate (%): The liquefaction rate was calculated according to the following formula:

Liquefaction rate [%] = ((Preparation weight of raw material [g] × (100 - moisture content) [%] - Dry weight of residue [g]) / (Preparation weight of raw material [g] × (100 - moisture content) [%]) × 100

Total organic carbon (TOC): TOC was determined using a TOC meter [TOC-V SCH; SHIMADZU (Kyoto Japan)]. The method is based on a 50-fold dilution of the liquefied material (1 mL of liquefied material in a measuring flask is metered up to 50 mL with distilled water).

Protein concentration (g/100 mL): Total nitrogen (mg/L) was analyzed using the Kjeldahl method. The nitrogen conversion factor was 6.25.

Lipid concentration (g/100 mL): Lipid concentration was analyzed by the liquid-liquid extraction method [13].

Carbohydrate concentration (g/100 mL) Calculation Formula: Total mass = Moisture - Protein - Lipid - Ash

Ash concentration (g/100 mL): Ash concentration was determined using the direct ashing method [14].

Acidity concentration (g/100 mL): Acidity concentration was determined using the titration method [15].

Caloric value (kcal/100 mL): Caloric value was determined using the modified Atwater method [16].

Results and Discussion

Subcritical water liquefaction of rice bran

For rice bran, we aimed to elute high concentrations of various components by treatment at temperatures higher than 180°C. The liquefaction rate and pH results are shown in table 2. The highest liquefaction rate was achieved by treatment at 180°C. The liquefaction rate decreased as the treatment temperature increased. The reason for the decrease in liquefaction rate at 200 and 220°C, at which the treatment capacity was originally higher, can be attributed to the carbonization of cellulose, which is abundantly contained in rice bran. The pH also decreased at higher temperatures. The decomposition of the abundant carbohydrates in rice bran, from monosaccharides to organic acids, is thought to have caused the decrease in pH.

Figure 3 shows the carbon content in the solid residue and subcritical water liquefied product at 200 and 220°C. The organic carbon concentration in the aqueous phase decreased

Table 2: Liquefaction rate and pH of subcritical water liquefied rice bran

Raw materials	Liquefaction rate [%]			pH		
	180°C	200°C	220°C	180°C	200°C	220°C
30 g	68.2	66.74	55.74	4.78	3.57	3.53
45 g	69.44	64.19	54.67	4.62	3.41	3.63
60 g	67.17	56.8	48.58	4.34	3.26	3.74

with increasing temperature. On the other hand, the carbon concentration in the solid residue increased in a temperature-dependent manner. From these two results, it can be inferred that the carbohydrates in rice bran, especially amorphous polysaccharides and cellulose in particular, underwent hydrolysis to saccharification and further aromatization (formation of furan compounds) during the treatment process, and became insoluble due to recombination (Maillard reaction and cross-linking) in the reactor [17-20]. In the future, we will conduct quantitative analysis of sugars, organic acids, and furan compounds to elucidate the reaction pathway.

Next, the results of amino acid analysis per unit mass are shown in figure 4. Although no significant differences were observed, slightly more efficient results were achieved at lower raw material weights.

Next, figure 5 shows the results of phosphorus and mineral components per unit mass. Here as well, no significant differences were observed, and slightly more efficient results were achieved at lower substrate weights.

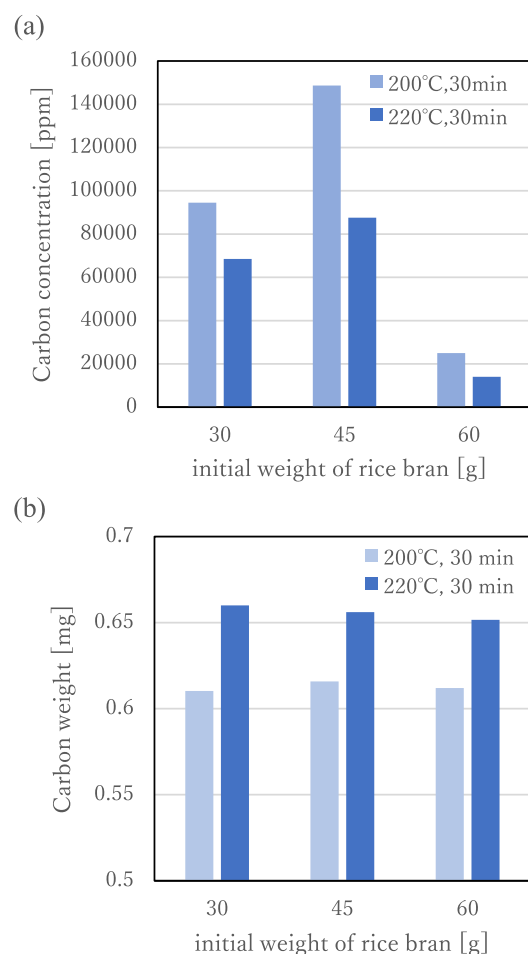


Figure 3: Carbon contents in the solid residue and subcritical water fractions

- (a) Carbon concentration of liquid fraction
- (b) Carbon weight of insoluble fraction

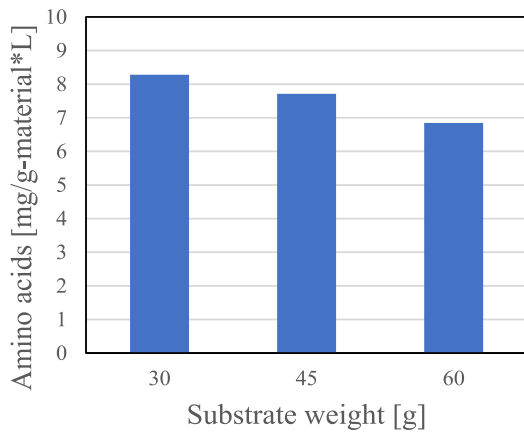


Figure 4: Results of amino acid analysis per unit mass

From these results, it was concluded that treatment at 180°C was the most suitable from the standpoint of processing efficiency; the water solubilization rate decreased under temperature conditions of 200°C or higher. The highest elution amount per unit mass was obtained at 30 g substrate weight. However, “45 g substrate weight” was selected as the optimal condition, as this condition ensured the elution of phosphorus and minerals comparable to the target “black vinegar” and had a relatively high elution efficiency.

Acetic acid fermentation of the subcritical water treated solution

In previous studies [1,2], the authors performed subcritical water treatment of sake lees (temperature 120°C, treatment time 240 min) and acetic acid fermentation of the liquefied product. The results showed a greater concentration of total amino acids compared to commercial black vinegar, yet the amounts of phosphorus and mineral components were inferior. In this experiment, we aimed to produce vinegar containing high concentrations of phosphorus and mineral components as well as amino acids by using rice bran as a source of phosphorus and mineral components. Specifically, subcritical water-treated sake lees and rice bran under their respective optimal conditions (sake lees: 120°C, 240 min; rice bran: 180°C, 30 min) were mixed 1:1 on a volume basis, and vinegar was produced by static fermentation for 3 days (hereafter referred to as mixed vinegar). Various analyses were then performed and the results are shown in table 3. The acidity of the mixed vinegar was 4.68%, which cleared the acidity specified in the JAS standard, and vinegar was successfully produced, albeit at the laboratory level.

Other analyses were also performed on this mixed vinegar in comparison to commercial products and sake lees vinegar (Figure 6). The amino acid content of the mixed vinegar was higher than that of the commercial products, which is a positive result. The mineral content was significantly higher compared to sake lees vinegar, but was not as high as black vinegar. Through a series of acetic acid fermentation

processes, it was confirmed that the subcritical water-treated products made from sake lees and rice bran did not interfere with each other even when mixed, and each of them retained high concentrations of nutrients.

Conclusions

The purpose of this study was to liquefy sake lees and rice bran by subcritical water treatment to produce a liquefied product rich in amino acids and minerals, and apply the liquefied product to the production of a new vinegar. In their previous studies[1,2], the authors found that subcritical water treatment of sake lees at 120°C for 240 min produced a liquefied product rich in amino acids. In the present study, subcritical treatment of rice bran at 180°C for 30 min

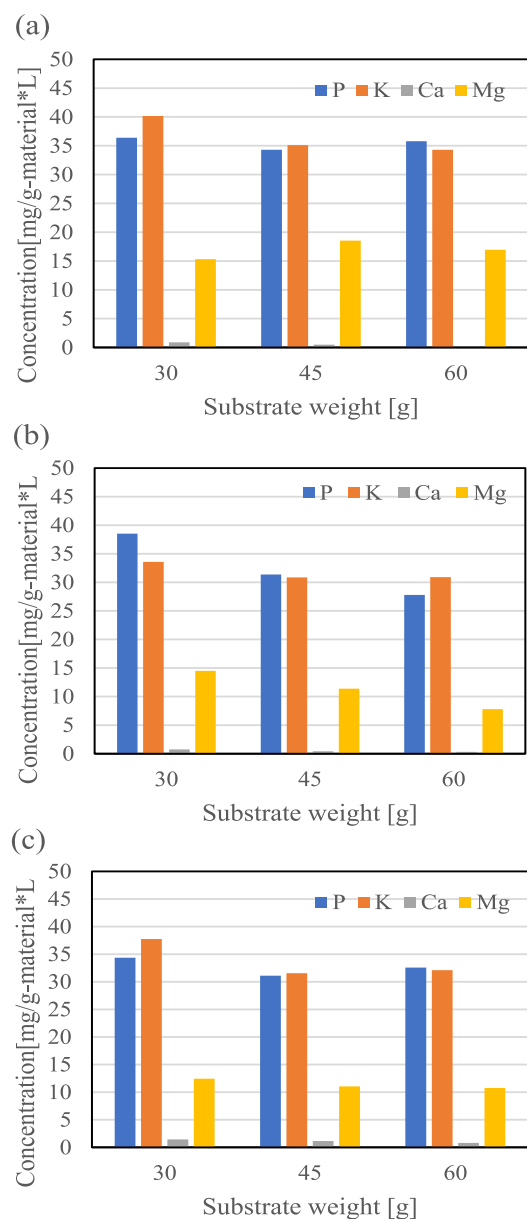


Figure 5: Phosphorus and mineral components per unit mass. (a) 180°C, 30min (b) 200°C, 30min (c) 220°C, 30min

Table 3: Nutritional analysis of the prepared vinegar (per 100mL)

	Energy (kcal)	Protein (g)	Lipids (g)	Carbohydrate (g)	Mineral content (g)	Acidity (g)
Mixed sample (1:1)	34	1.4	0	8.3	0.4	4.68
Sake lees 120°C,240min	25	1.7	0	5.7	0.1	4.39
Grain vinegar	26	0.4	0	7.1	0.1	4.26

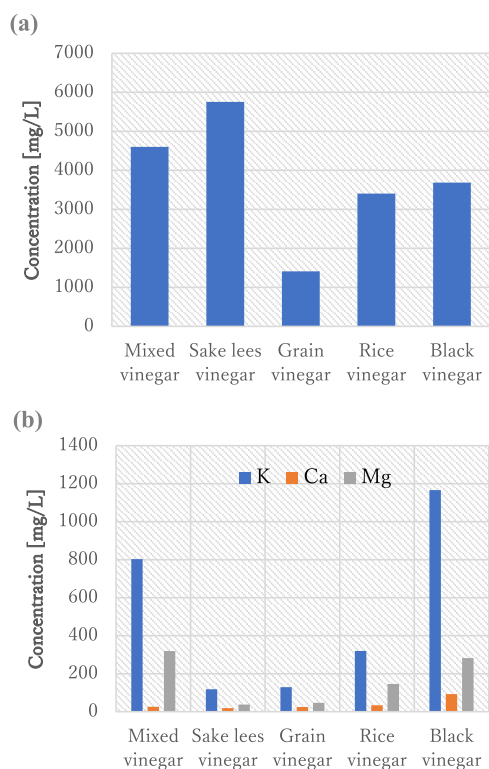


Figure 6: Comparison of the components of various vinegars. (a) Comparison of contained amino acids (b) Comparison of contained minerals

produced a liquefied product rich in mineral components. The subcritical water liquefied rice bran was mixed with the subcritical water liquefied sake lees at a ratio of 1:1, and acetic acid fermentation was carried out. As a result, a vinegar with high nutritional value, similar to commercially-available black vinegar, was produced. This experiment also suggested that the nutrient content of the vinegar could be controlled by changing the mixing ratio of sake lees and rice bran subcritical water-treated samples. We aim to conduct future experiments with different mixing ratios.

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Conflict of interests

The authors declare that they have no conflict of interests.

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